



Eco-profiles and Environmental Product Declarations of the European Plastics Manufacturers

Styrene Acrylonitrile (SAN) and Acrylonitrile Butadiene Styrene (ABS)

PlasticsEurope
February 2015



PlasticsEurope
Association of Plastics Manufacturers

Table of Content

Table of Content.....	2
Environmental Product Declaration.....	3
Introduction.....	3
Meta Data.....	3
Description of the Product and the Production Process.....	3
Environmental Performance.....	4
Additional Environmental and Health Information	5
Additional Technical Information	5
Additional Economic Information.....	5
Information	6
Goal & Scope.....	7
Intended Use & Target Audience	7
Product Category and Declared Unit.....	8
Product and Producer Description	8
Eco-profile – Life Cycle Inventory	10
System Boundaries	10
Cut-off Rules	11
Data Quality Requirements	11
Calculation Rules	14
Life Cycle Inventory (LCI) Results.....	15
Life Cycle Impact Assessment	27
Input	27
Output.....	27
Reviews.....	32
Internal Independent Quality Assurance Statement.....	32
External Independent Review Summary	33
References.....	33

Environmental Product Declaration

Introduction

This Environmental Product Declaration (EPD) is based upon life cycle inventory (LCI) data from the GaBi database 2013 fulfilling the requirements on PlasticsEurope's Eco-profile programme. It has been prepared according to **PlasticsEurope's Eco-profiles and Environmental Declarations – LCI Methodology and PCR for Uncompounded Polymer Resins and Reactive Polymer Precursors** (PCR version 2.0, April 2011). EPDs provide environmental performance data, but no information on the economic and social aspects which would be necessary for a complete sustainability assessment. EPDs do not imply a value judgment between environmental criteria.

This EPD describes the production of Styrene Acrylonitrile (SAN) and Acrylonitrile Butadiene Styrene (ABS) from cradle to gate (from crude oil extraction to granules or resin at plant, i.e. SAN and ABS production site output). **Please keep in mind that comparisons cannot be made on the level of the polymer material alone:** it is necessary to consider the full life cycle of an application in order to compare the performance of different materials and the effects of relevant life cycle parameters. This EPD is intended to be used by member companies, to support product-orientated environmental management; by users of plastics, as a building block of life cycle assessment (LCA) studies of individual products; and by other interested parties, as a source of life cycle information.

Meta Data

Data Owner	PlasticsEurope aisbl
LCA Practitioner	PE INTERNATIONAL AG
Programme Owner	PlasticsEurope aisbl
Programme Manager, Reviewer	DEKRA Assurance Services GmbH
Number of plants included in data collection	5 (SAN/AMSAN) 5 (ABS)

¹ Comparing the (confidential) foreground data for AMSAN and SAN regarding energy demand and the overall results of the main impact categories, both production routes do not show significant differences outside the range of variation of all single results.

Representativeness	90%
Reference year	2013
Year of data collection and calculation	2014
Expected temporal validity	2023
Cut-offs	No significant cut-offs
Data Quality	Good
Allocation method	None

Description of the Product and the Production Process

Styrene Acrylonitrile (SAN) is a co-polymer with statistical repetition of styrene and acrylonitrile units in the polymer chain. The described average product comes from materials with about 75% styrene and 25% acrylonitrile (in mass%). A variant using Alpha Methyl Styrene (AMS) as a monomer also exists: AMSAN. This material is included in the average calculation¹.

Acrylonitrile Butadiene Styrene (ABS) is a thermoplastic 2 phase-polymer. The proportions of the monomer components can vary. This Eco-profile covers an average of product compositions of about 45-65% styrene, 15-20% acrylonitrile and 10-25% butadiene (in mass%).

The co-polymerisation of styrene with further monomers leads to materials which show advantages compared to polystyrene with regard to hardness, strength, resistance to heat distortion and environmental stress cracking.

Production Process

For the production of SAN/AMSAN, suspension and continuous bulk technologies are applied; ABS is produced by emulsion polymerisation, bulk polymerisation or combined processes. The type of production technology influences the material's properties. While Mass ABS process is mainly used

for General purpose ABS applications with excellence flow/hardness performance, emulsion polymerization is preferred to produce ABS products with high gloss and toughness requirements. The full range of ABS properties for injection molding and extrusion processing is available when products made by different technologies are mixed in compounding.

The reference flows, to which all data given in this EPD refer, are 1 kg SAN/AMSAN granulates and 1 kg of ABS granulates, respectively.

Data Sources and Allocation

The main data source is a primary data collection from European producers of SAN/AMSAN and ABS, providing site-specific gate-to-gate production data for processes under operational control of the four participating companies.

Each participant of the study delivered data for SAN and ABS production. Overall four sites for SAN production, one for AMSAN and five sites for ABS production are included in the average calculations.

This covers more than 90 % of the European SAN and ABS production (EU-27) in 2013, respectively. The data for the precursors upstream supply chain (styrene, alpha-methyl styrene, acrylonitrile and butadiene) are taken from the database of the software system GaBi 6 [GABI 6]. A mix of two different routes for the production of styrene (EBSM and POSM) is modelled. All relevant background data, such as energy and auxiliary materials, is from the GaBi 6 database; the documentation is publicly available [GABI 6].

Use Phase and End-of-Life Management

SAN is marketed for a range of applications such as cookware, transparent parts in electronics and electrical appliances, instrument panels, sanitary and medical goods or cosmetic packaging. SAN can also be used as the rigid component for ABS manufacturing. AMSAN is used as a modifier for increasing the heat resistance of ABS and PVC.

Due to its combination of strength and impact resistance, ABS is widely used as an engineering

material. The main consumers are the automotive industry, the domestic appliances industry, the data technology and telecommunications area, and producers of refrigeration equipment, toys, sports articles, and semi-finished articles.

SAN and ABS can be recycled, used articles can be ground and directly recycled in the production process. Furthermore, energy recovery by incineration is also possible.

Environmental Performance

The tables below show the environmental performance indicators associated with the production of 1 kg SAN and 1 kg of ABS.

Input Parameters

Indicator	Unit	Value	
		SAN	ABS
Non-renewable energy resources ¹⁾	MJ	91.61	90.57
• Fuel energy	MJ	48.21	47.34
• Feedstock energy	MJ	43.40	43.23
Renewable energy resources (biomass) ¹⁾	MJ	1.27	1.61
• Fuel energy	MJ	0.67	0.84
• Feedstock energy	MJ	0.60	0.77
Abiotic Depletion Potential			
• Elements	kg Sb eq	8.87E-07	1,48E-06
• Fossil fuels	MJ	82.93	81,37
Renewable materials (biomass)	kg	-	-
Water use (key foreground process level)	kg	21.76	22.03
• for process	kg	na	na
• for cooling	kg	na	na

¹⁾ Calculated as upper heating value (UHV)
na= not available – details see table 17/18

Output Parameters

Indicator	Unit	Value	
		SAN	ABS
GWP	kg CO ₂ eq	2.96	3.10
ODP	g CFC-11 eq	8.32E-08	2.60E-07
AP	g SO ₂ eq	8.04	7.69
POCP	g Ethene eq	1.19	1.09
EP	g PO ₄ eq	1.02	1.03
Dust/particulate matter ²⁾	g PM10	1,37E-04	2,35E-04
Total particulate matter ²⁾	g	2,13E-01	2.39E-01
Waste			
• Radioactive waste	kg	6.15E-04	8.58E-04
• Non-radioactive waste ³⁾	kg	1.98E-02	2.86E-02

²⁾ Including secondary PM10

³⁾ Non-radioactive wastes include: spoil, tailings, and waste, deposited

Additional Environmental and Health Information

SAN and ABS can be safely used in toy and medical appliances manufacturing as well as for food processing applications.

Additional Technical Information

Chemical resistance, mechanical strength and transparency are the main properties of SAN. In addition, AMSAN offers a higher heat resistance.

For ABS, the polybutadiene rubber inclusions in the polymer matrix provide enhanced mechanical properties, such as toughness and impact resistance. Due to high stiffness and low density, all articles made from SAN/AMSAN and ABS have excellent strength-to-weight ratio.

Additional Economic Information

The technical properties chemical and impact resistance and strength for ABS and SAN enables the application in many areas. Weight reduction offers improvement potentials in applications for e.g. automotive parts, household appliances or safety helmets.

Information

Data Owner

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E-mail: info@plasticseurope.org.

Programme Manager & Reviewer

DEKRA Assurance Services GmbH

This Environmental Product Declaration has been reviewed by DEKRA Assurance Services GmbH. It was approved according to the Product Category Rules PCR version 2.0 (2011-04) and ISO 14025:2006.
Registration number: PlasticsEurope 2015-003, validation expires on 31 December 2017 (date of next revalidation review).

Programme Owner

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For copies of this EPD, for the underlying LCI data (Eco-profile); and for additional information, please refer to <http://www.plasticseurope.org/>.

References

PlasticsEurope: Eco-profiles and environmental declarations – LCI methodology and PCR for uncompounded polymer resins and reactive polymer precursors (version 2.0, April 2011).

Goal & Scope

Intended Use & Target Audience

Ø Eco-profiles (LCIs) and EPDs from this programme are intended to be used as »cradle-to-gate« building blocks of life cycle assessment (LCA) studies of defined applications or products. LCA studies considering the full life cycle (»cradle-to-grave«) of an application or product allow for comparative assertions to be derived. It is essential to note that comparisons cannot be made at the level of the polymer or its precursors. In order to compare the performance of different materials, the whole life cycle and the effects of relevant life cycle parameters must be considered.

PlasticsEurope Eco-profiles and EPDs represent polymer production systems with a defined output. They can be used as modular building blocks in LCA studies. However, these integrated industrial systems cannot be disaggregated further into single unit processes, such as polymerisation, because this would neglect the interdependence of the elements, e.g. the internal recycling of feedstocks and precursors between different parts of the integrated production sites.

PlasticsEurope Eco-profiles and EPDs are prepared in accordance with the stringent ISO 14040–44 requirements. Since the system boundary is »cradle-to-gate«, however, their respective reference flows are disparate, namely referring to a broad variety of polymers and precursors. This implies that, in accordance with ISO 14040–44, a direct comparison of Eco-profiles is impossible. While ISO 14025, Clause 5.2.2 does allow EPDs to be used in comparison, PlasticsEurope EPDs are derived from Eco-profiles, i.e. with the same »cradle-to-gate« system boundaries.

As a consequence, a direct comparison of Eco-profiles or EPDs makes no sense because 1 kg of different polymers are not functionally equivalent.

Once a full life cycle model for a defined polymer application among several functionally equivalent systems is established, and only then, can comparative assertions be derived. The same goes for EPDs, for instance, of building product where PlasticsEurope EPDs can serve as building blocks.

Eco-profiles and EPDs are intended for use by the following target audiences:

- member companies, to support product-orientated environmental management and continuous improvement of production processes (benchmarking);
- downstream users of plastics, as a building block of life cycle assessment (LCA) studies of plastics applications and products; and
- other interested parties, as a source of life cycle information.

Product Category and Declared Unit

Product Category

The core product category is defined as **uncompounded polymer resins and reactive polymer precursors**. This product category is defined »at gate« of the polymer or precursor production and is thus fully within the scope of PlasticsEurope as a federation. In some cases, it may be necessary to include one or several additives in the Eco-profile to represent the polymer or precursor »at gate«. For instance, some polymers may require a heat stabiliser, or a reactive precursor may require a flame retardant. This special case is distinguished from a subsequent compounding step conducted by a third-party downstream user (outside PlasticsEurope's core scope).

Functional Unit and Declared Unit

The default Functional Unit and Declared Unit of PlasticsEurope Eco-profiles and EPDs are (unless otherwise specified²):

1 kg of Styrene Acrylonitrile (SAN) / Alpha Methyl Styrene Acrylonitrile (AMSAN) – or – 1 kg of Acrylonitrile Butadiene Styrene granules (ABS), respectively, »at gate« (production site output) representing a European industry production average.

Product and Producer Description

Product Description

Styrene Acrylonitrile (SAN) / Alpha Methyl Styrene Acrylonitrile (AMSAN) and Acrylonitrile Butadiene Styrene (ABS) are thermoplastic polymers, used in many applications such as cookware, electronics and electrical appliances, automotive parts, instrument panels, sanitary and medical goods or cosmetic packaging, toys...

Styrene Acrylonitrile (SAN)

CAS no. 9003-54-7

Chemical formula $(C_8H_8)_x (C_3H_3N)_y$

Gross calorific value ca. 40 MJ/kg

Alpha-Methyl Styrene Acrylonitrile (AMSAN)

CAS no. 25747-74-4

Chemical formula $(C_9H_{10})_x (C_3H_3N)_y$

Gross calorific value ca. 40 MJ/kg

Acrylonitrile Butadiene Styrene (ABS)

CAS no. 9003-56-9

Chemical formula $(C_8H_8)_x (C_4H_6)_y \cdot (C_3H_3N)_z$

Gross calorific value ca. 40 MJ/kg

² Exceptions can occur when reporting Eco-profiles of, for instance, process energy, such as on-site steam, or conversion processes, such as extrusion.

Production Process Description

Styrene Acrylonitrile (SAN) and Alpha-Methyl Styrene Acrylonitrile (AMSAN) are most commonly made using a bulk polymerisation process. The process consists of continuous feeds of the monomers as well as possibly initiators chain transfer agents and solvent, to one or more polymerisation reactors. Polymerisation takes place between 80 and 170°C; adequate agitation is critical for proper temperature and composition control. The product then goes to devolatilisation units and pelletiser. Unreacted monomers are recycled to maintain conversion and composition at desired levels.

Acrylonitrile Butadiene Styrene (ABS) can be produced by emulsion polymerisation, bulk polymerisation or combined processes. In the first, ABS graft rubber and SAN matrix are either polymerised separately then compounded, or polymerised together. The second starts with butadiene rubber in solvent, followed by a pre-polymerisation of the rubber-monomers mixture under continuous mixing. The polymerisation is finally completed; the product is centrifuged, dried and compounded.

For SAN or ABS sold to the market, additives such as lubricants, antioxidants or light stabilisers can also be added.

Producer Description

PlasticsEurope Eco-profiles and EPDs represent European industry averages within the scope of PlasticsEurope as the issuing trade federation. Hence they are not attributed to any single producer, but rather to the European plastics industry as represented by PlasticsEurope's membership and the production sites participating in the Eco-profile data collection. The following companies contributed to provide data to this Eco-profile and EPD:

§ Elix Polymers S.L.
Apartado Correos 176
43080 Tarragona
Spain
<http://www.elix-polymers.com>

§ Styrolution Group GmbH
Erlenstrasse 2
60325 Frankfurt am Main
Germany
<http://www.styrolution.com>

§ Styron Europe GmbH
Herber H. Dowweg5, 4542 NM HOEK
4530 AA Terneuzen
The Netherlands
<http://www.styron.com>

§ VERSALIS S.p.A.
Piazza Boldrini, 1
20097 San Donato Milanese (MI)
Italy
<http://www.versalis.eni.com>

Eco-profile – Life Cycle Inventory

System Boundaries

PlasticsEurope Eco-profiles and EPDs refer to the production of polymers as a cradle-to-gate system (see Figure 1).

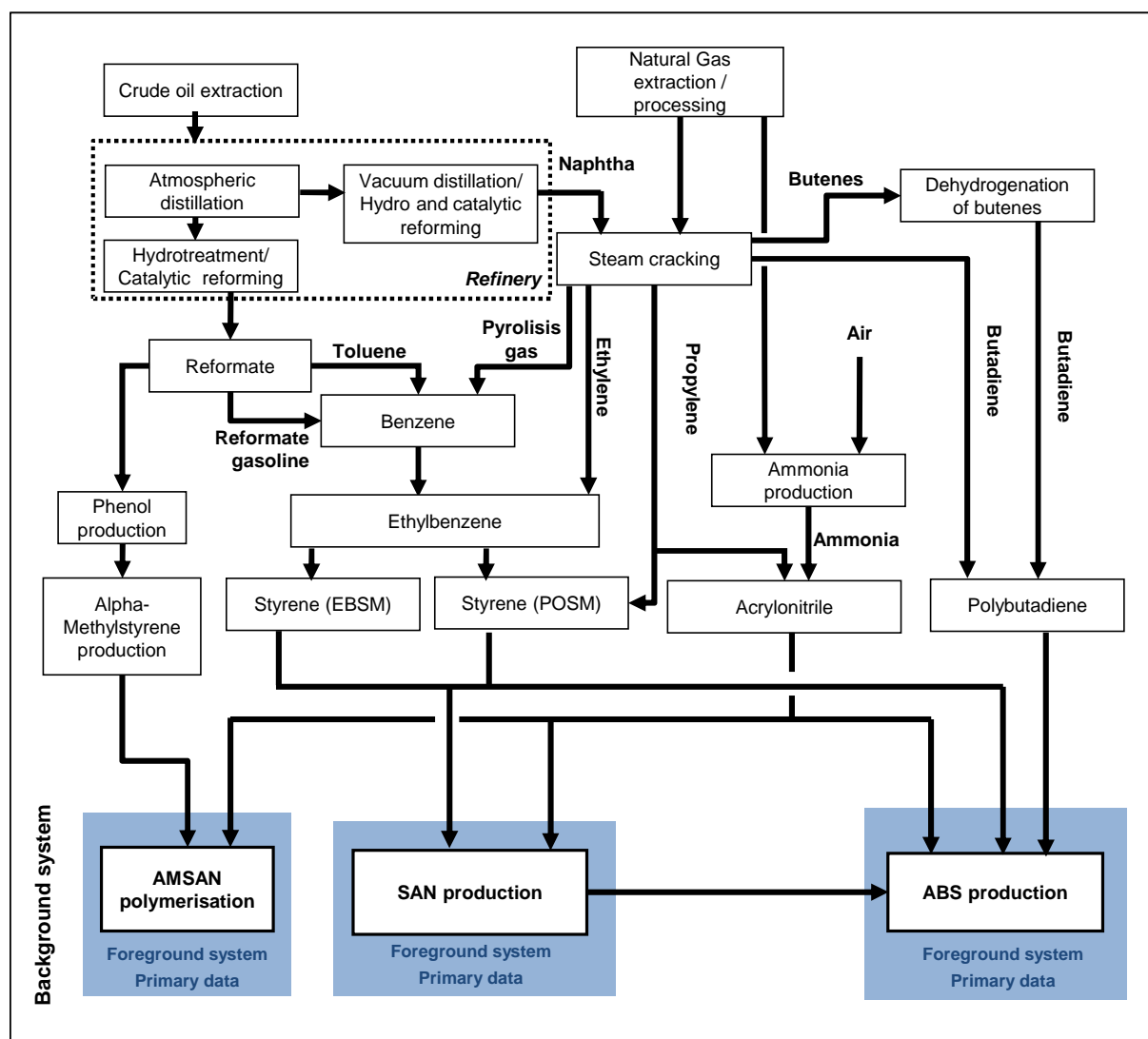


Figure 1: Cradle-to-gate system boundaries (SAN/AMSAN and ABS)

Technological Reference

The production processes are modelled using specific values from primary data collection at site. The main data source is a primary data collection from European producers of SAN/AMSAN and ABS, providing site-specific gate-to-gate production data for processes under operational control of the participating companies: four SAN and one AMSAN producers with five plants in four different European countries; five ABS producers with five plants in five European countries. This covers 90% of the European SAN/AMSAN and ABS production capacity (EU-27) in 2013, respectively. Primary data are used for all foreground processes (un-

der operational control) complemented with secondary data for background processes (under indirect management control). The data for the upstream supply chain until the precursors are taken from the database of the software system GaBi 6 [GaBi 6].

As shown in Figure 1, two different routes for the production of styrene (EBSM and POSM) are modelled. The ethylbenzene styrene monomer (EBSM) process is based on the catalytic dehydrogenation of ethylbenzene and renders styrene as its main product and minor quantity of toluene as co-product. The propylene oxide styrene monomer (POSM) process involves the co-production of propylene oxide and styrene: in this case, ethylbenzene is oxidized to form ethylbenzene hydroperoxide (EBHP). The use of one or a mixture of both technologies is modelled according to site-specific information or as an assumption of a 50/50 mix as far as information is available.

Temporal Reference

The LCI data for production is collected as 12 month averages representing the year 2013, to compensate seasonal influence of data. Background data have reference years 2012 and 2010 for electricity and thermal energy processes. The dataset is considered to be valid until substantial technological changes in the production chain occur. In view of the latest technology development, the overall reference year for this Eco-profile is 2013, with a maximum temporal validity until 2023 for the foreground system.

Geographical Reference

Primary production data for both SAN/AMSAN and ABS production are from four different European suppliers each. The inventories for the precursors and the energy supply are adapted according to site specific (i.e. national) conditions. Inventories for the group of "Other chemicals", used in smaller amounts, refer to European conditions or geographical conditions as the datasets are available. Therefore, the study results are intended to be applicable within EU boundaries: adjustments might be required if the results are applied to other regions. SAN and ABS imported into Europe are not considered in this Eco-profile.

Cut-off Rules

In the foreground processes all relevant flows are considered, trying to avoid any cut-off of material and energy flows. In single cases additives used in the SAN and/or ABS foreground unit process (<0.3% m/m of product output) are neglected. In such cases, it is assured that no hazardous substances or metals are present in this neglected part. According to the GaBi database [GaBi 6], used in the background processes, at least 95% of mass and energy of the input and output flows are covered and 98% of their environmental relevance (according to expert judgment) are considered, hence an influence of cut-offs less than 1% on the total is expected. Transports for the main input materials (styrene, alpha-methyl styrene, acrylonitrile and butadiene) contribute less than 3% to the overall environmental burden. The contribution of transport of small material proportions is expected to be less than 1%; hence the transports for minor input amounts are excluded.

Data Quality Requirements

Data Sources

Eco-profile and EPDs developed by PlasticsEurope use average data representative of the respective foreground production process, both in terms of technology and market share. The primary data are derived

from site specific information for processes under operational control supplied by the participating member companies of PlasticsEurope (see Producer Description).

The data for the upstream supply chain are taken from the life cycle database of the software system GaBi [GaBi 6]. Most of the background data used is publicly available and public documentation exists.

Styrene as a relevant intermediate originates from two different technology routes.

EBSM (ethyl benzene styrene monomer) is based on catalytic dehydrogenation of ethylbenzene, with styrene as its main product. The process for POSM (propylene oxide-styrene monomer) involves the oxidation of ethylbenzene; the process delivers styrene and propylene oxide.³

The environmental impacts of these two styrene production routes show differences of about 10%; this is in the range of common uncertainty conducting an LCA.

Both production routes are mainly based on benzene as a precursor for ethylbenzene. Benzene again is a product of different technology routes, which influences significantly the environmental burden in the supply chain. The applied data refer to the European mix based on current data on market availability of benzene by Petrochemicals Europe (Association of petrochemical producers): major benzene supply originates from pyrolysis gas (about 55%), about one third is produced via reformat production; the leftover proportion of 15% is produced via coal based production and toluene derivatives.

The propylene inventory used in the POSM-route reflects the main production route from steam cracking.

The eco-profile methodology instructs the general principle to use existing eco-profile data for modelling the supply chain. However, the life cycle inventory for butadiene, published by PlasticsEurope (2012), causes inter-operability issues when converted into the international ILCD standard, a necessary step to enable the integration in any other LCA software system (such as e.g. GaBi). According to the foreground data, different types of butadiene (as monomer and also pre-polymerised) are used and regionalised data are to be favoured whenever possible. This situation induced the decision to use consistent and regionalised inventory data provided by the GaBi database, including butadiene and its pre-polymer.

The butadiene GaBi dataset is based on robust information for the petrochemical supply chain. Refinery processes, steam cracker and chemical refinement are well elaborated technologies with high efficiencies and proven techniques. Technical background information is described in standard references like Ullmann's etc.. Thermodynamic calculations accompanied by engineering expertise allowed the conversion into life cycle inventories for the GaBi database..

As far as ABS Eco-profile LCIA results are concerned, the sensitivity analysis between the GaBi vs. PlasticsEurope butadiene inventories results in differences of less than 10% on the overall values for the considered impact categories.

Relevance

With regard to the goal and scope of this Eco-profile, the collected primary data of foreground processes are of high relevance, i.e. data was sourced from the most important SAN and ABS producers in Europe in order to generate a European production average. The environmental contributions of each process to the overall LCI results are included in the Chapter 'Life Cycle Impact Assessment'.

³ More details on EBSM-POSM technology can be found in the Eco-profile "General-Purpose Polystyrene (GPPS) and High-Impact Polystyrene (HIPS), Registration number: PlasticsEurope 2012-004

Representativeness

The participating companies represent 90% of the European SAN and ABS production volume in 2013. This figure refers to an educated estimate of PlasticsEurope and the participating parties of this study. The selected background data can be regarded as representative for the intended purpose.

Consistency

To ensure consistency, only primary data of the same level of detail and background data from the GaBi 6 databases [GaBi 6] are used. While building up the model, cross-checks ensure the plausibility of mass and energy flows. The methodological framework is consistent throughout the whole model as the same methodological principles are used both in the foreground and background systems. In addition to the external review, an internal independent quality check was performed (see 'Internal Independent Quality Assurance Statement').

Reliability

Data of foreground processes provided directly by producers are predominantly measured. Data of relevant background processes are measured at several sites – alternatively, they are determined from literature data, or estimated for some flows, which usually have been reviewed and quality checked.

Completeness

Primary data used for the gate-to-gate production of SAN and ABS covers all related flows in accordance with the above cut-off criteria. In this way all relevant flows are quantified and data is considered complete. The elementary flows covered in the model enable the impact assessment of all selected impact categories. Waste treatment is included in the model, so that only elementary flows cross the system boundaries.

Precision and Accuracy

As the relevant foreground data is primary data, or modelled based on primary information sources of the owners of the technologies, precision is deemed appropriate to the goal and scope.

Reproducibility

Reproducibility is given for internal use since the owners of the technologies provided the data under confidentiality agreements. Key information is documented in this report, and data and models are stored in the GaBi 6 software database. Sub-systems are modelled by 'state of art' technology using data from a publicly available and internationally used database. It is worth noting that for external audiences, full and detailed reproducibility will not be possible for confidentiality reasons. However, experienced practitioners could reproduce suitable parts of the system as well as key indicators in a certain confidence range.

Data Validation

The data on production collected by the project partners and the data providing companies are validated in an iterative process several times. The collected data are validated using existing data from published sources or expert knowledge. The background information from the GaBi database is updated regularly and continuously validated.

Life Cycle Model

The study is performed with the LCA software GaBi 6 [GABI 6]. The associated database integrates ISO 14040/44 requirements. Due to confidentiality reasons details on software modelling and methods used cannot be shown here. However, provided that appropriate confidentiality agreements are in place the model can be reviewed in detail; an external independent review has been conducted to this aim. The calculation follows the vertical calculation methodology (see below).

Calculation Rules

Vertical Averaging

When modelling and calculating average Eco-profiles from the collected individual LCI datasets, vertical averages are calculated (Figure 2).

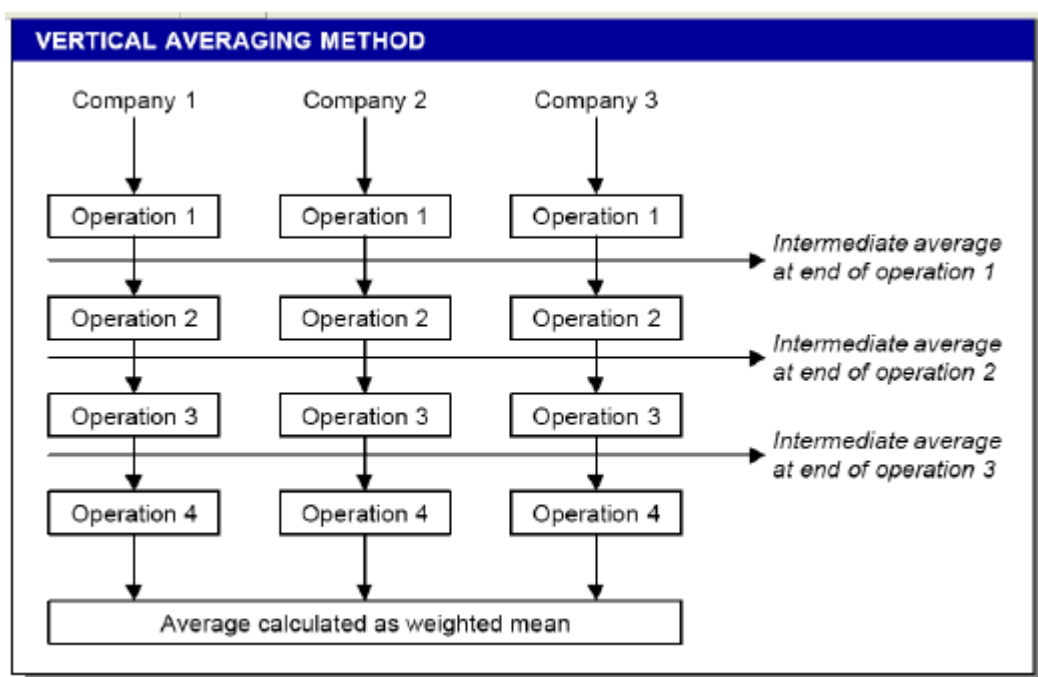


Figure 2: Vertical Averaging (source: Eco-profile of high volume commodity phthalate esters, ECPI (European Council for Plasticisers and Intermediates, 2001))

Allocation Rules

Production processes in chemical and plastics industry are usually multi-functional systems, i.e. they have not one, but several valuable product and co-product outputs. Wherever possible, allocation should be avoided by expanding the system to include the additional functions related to the co-products. Often, however, avoiding allocation is not feasible in technical reality, as alternative stand-alone processes do not exist or even alternative technologies show completely different technical performance and product quality output. In such cases, the aim of allocation is to find a suitable partitioning parameter so that the inputs and outputs of the system can be assigned to the specific product sub-system under consideration.

Foreground system

In some companies' information, output material with deviations from the required specification is reported. If these materials show only slight differences and are sold at comparable price-level, they are assumed as

product output (< 4% of total production); in case of material declared as off-grade sent to recovery, neither further environmental burden nor credits are given to the modelled system (< 1% of total production). No post-consumer waste is reported as input to the system, therefore no allocation between different life cycles is necessary.

Background system

In the refinery operations, co-production is addressed by applying allocation based on mass and net calorific value [GABI 6]. The chosen allocation in downstream petrochemicals is based on several sensitivity analyses, which were reviewed by petrochemical experts. Materials and chemicals needed are modelled using the allocation rule most suitable for the respective product (mass, energy, exergy, economic). For further information on specific product see documentation.gabi-software.com.

Life Cycle Inventory (LCI) Results

Formats of LCI Dataset

The Eco-profile is provided in four electronic formats:

- § As input/output table in Excel®
- § As XML document in EcoSpold format (www.ecoinvent.org)
- § As XML document in ILCD format (<http://lct.jrc.ec.europa.eu>)
- § As LCI in GaBi format (www.gabi-software.com)

Key results are summarised below.

Energy Demand

As a key indicator on the inventory level, the **primary energy demand** (system input) of 92.88 MJ/kg SAN and 92.18 MJ/kg ABS indicates the cumulative energy requirements at the resource level, accrued along the entire process chain (system boundaries), quantified as gross calorific value (upper heating value, UHV).

As a measure of the share of primary energy incorporated in the product, and hence indicating a recovery potential, the **energy content in the polymer** (system output), quantified as the gross calorific value (UHV), is about 40 MJ/kg for SAN and ABS.

Table 1: Primary energy demand (system boundary level) per 1 kg SAN

Primary Energy Demand	Value [MJ]
Energy content in polymer (energy recovery potential, quantified as gross calorific value of polymer)	40.00
Process energy (quantified as difference between primary energy demand and energy content of polymer)	52.88
Total primary energy demand	92.88

Table 2: Primary energy demand (system boundary level) per 1 kg ABS

Primary Energy Demand	Value [MJ]
Energy content in polymer (energy recovery potential, quantified as gross calorific value of polymer)	40.00
Process energy (quantified as difference between primary energy demand and energy content of polymer)	52.18
Total primary energy demand	92.18

Consequently, the difference (Δ) between primary energy input and energy content in polymer output is a measure of **process energy** which may be either dissipated as waste heat or recovered for use within the system boundaries.

Table 3 and Table 4 show how the total energy input (primary energy demand) is used as fuel or feedstock. Fuel use means generating process energy, whereas feedstock use means incorporating hydrocarbon resources into the polymer. Note that some feedstock input may still be valorised as energy; furthermore, process energy requirements may also be affected by exothermal or endothermal reactions of intermediate products. Hence, there is a difference between the feedstock energy input and the energy content of the polymer (measurable as its gross calorific value). Considering this uncertainty of the exact division of the process energy as originating from either fuels or feedstocks, as well as the use of average data (secondary data) in the modelling with different country-specific grades of crude oil and natural gas, the feedstock energy is presented as approximate data.

Table 3: Analysis by primary energy resources (system boundary level), expressed as energy and/or mass (as applicable) per 1 kg SAN

Primary energy resource input	Total Energy Input [MJ]	Total Mass Input [kg]	Feedstock Energy Input [MJ]	Fuel Energy Input [MJ]
Coal	1.49	0.05		1.49
Oil	50.09	1.11	25.15	24.94
Natural gas	37.55	0.77	18.85	18.70
Lignite	0.93	0.07		0.93
Nuclear	1.54	3.41E-06		1.54
Biomass	0.00			0.00
Hydro	0.27			0.27
Solar	0.54			0.54
Geothermics	6.79E-03			0.01
Waves	3.97E-13			0.00
Wood	3.65E-11			0.00
Wind	0.45			0.45
Other renewable fuels	0.00			0.00
Sub-total renewable	1.27	0.00	0.00	1.27
Sub-total Non-renewable	91.61	2.00	44.00	47.61
Total	92.88	2.00	44.00	48.88

Table 4: Analysis by primary energy resources (system boundary level), expressed as energy and/or mass (as applicable) per 1 kg ABS

Primary energy re-source input	Total Energy Input [MJ]	Total Mass Input [kg]	Feedstock Energy Input [MJ]	Fuel Energy Input [MJ]
Coal	1.71	0.06		1.71
Oil	47.72	1.06	24.41	23.31
Natural gas	38.28	0.78	19.59	18.70
Lignite	0.69	0.05		0.69
Nuclear	2.16	4.79E-06		2.16
Biomass	0.00			0.00
Hydro	0.27			0.27
Solar	0.98			0.98
Geothermics	1.18E-02			0.01
Waves	3.14E-13			0.00
Wood	2.89E-11			0.00
Wind	0.35			0.35
Other renewable fuels	0.00			0.00
Sub-total renewable	1.61	0.00	0.00	1.61
Sub-total Non-renewable	90.57	1.95	44.00	46.57
Total	92.18	1.95	44.00	48.18

Table 5 and Table 6 show that nearly all of the primary energy demand is from non-renewable resources. Since the focus scope of PlasticsEurope and their member companies is the polymer production, Table 7 and Table 8 analyse the types of useful energy inputs in the polymerisation process: electricity has a slightly minor contribution compared to thermal energy (heat). This represents the share of the energy requirement that is under operational control of the polymer producer (Figure 3). Accordingly, Table 9 and Table 10 show that the majority (96% for SAN, 94% for ABS) of the primary energy demand is accounted for by upstream processes. Finally, Table 11 and Table 12 provide a more detailed overview of the key processes along the production system, their contribution to primary energy demand and how this is sourced from the respective energy resources. This puts the predominant contribution of the production into perspective with the precursors (»precursors«). In order to analyse these upstream (pre-chain) operations more closely, please refer to the Eco-profiles and the GaBi documentation of the respective precursors. It should be noted, however, that the LCI tables in the annex account for the entire cradle-to-gate primary energy demand of the SAN and ABS system.

Table 5: Primary energy demand by renewability per 1 kg SAN

Fuel/energy input type	Value [MJ]	%
Renewable energy resources	1.27	1%
Non-renewable energy resources	91.61	99%
Total	92.88	100%

Table 6: Primary energy demand by renewability per 1 kg ABS

Fuel/energy input type	Value [MJ]	%
Renewable energy resources	1.61	2%
Non-renewable energy resources	90.57	98%
Total	92.18	100%

Table 7: Analysis by type of useful energy (production – key foreground process level) per 1 kg SAN

Type of useful energy in process input	Value [MJ]
Electricity	0.87
Heat, thermal energy	1.46
Other types of useful energy (relevant contributions to be specified)	0.00
Total (for selected key unit process)	2.34

Table 8: Analysis by type of useful energy (production – key foreground process level) per 1 kg ABS

Type of useful energy in process input	Value [MJ]
Electricity	1.06
Heat, thermal energy	1.61
Other types of useful energy (relevant contributions to be specified)	0.00
Total (for selected key unit process)	2.67

Table 9: Contribution to primary energy demand (dominance analysis) per 1 kg SAN

Contribution to Primary Energy per segment	Value [MJ]	%
Production (electricity, steam, unit process, utilities, waste treatment)	4.14	4%
Pre-chain	88.74	96%
Total	92.88	100%

Table 10: Contribution to primary energy demand (dominance analysis) per 1 kg ABS

Contribution to Primary Energy per segment	Value [MJ]	%
Production (electricity, steam, unit process, utilities, waste treatment)	5.68	6%
Pre-chain	86.50	94%
Total	92.18	100%

Table 11: Contribution of life cycle stages to total primary energy demand (gross calorific values) per 1 kg SAN, see Figure 3

Total Pri- mary Energy [MJ]	Precursors	Other Chemicals	Utilities	Electricity	Thermal Energy	Transport	Process Waste Treatment
Coal	1.16	0.01	0.02	0.32	2.81E-03	4.96E-03	-0.03
Oil	49.81	0.06	7.22E-03	0.10	5.75E-03	0.11	-4.96E-03
Natural gas	35.06	0.12	0.03	0.74	1.78	0.02	-0.21
Lignite	0.60	0.01	0.02	0.31	1.73E-03	4.20E-03	-0.02
Nuclear	1.06	0.01	0.04	0.47	3.32E-03	8.84E-03	-0.05
Biomass	0.00	0.00	0.00	0.00	0.00	0.00	0.00
Hydro	0.17	1.89E-03	7.91E-03	0.09	8.72E-04	1.70E-03	-0.01
Solar	0.32	0.04	7.24E-03	0.18	1.37E-03	2.37E-03	-8.24E-03
Geothermics	4.67E-03	3.91E-05	3.43E-04	2.10E-03	3.98E-05	7.41E-05	-4.79E-04
Waves	2.37E-13	3.83E-15	4.21E-15	1.54E-13	1.00E-15	8.34E-16	-3.86E-15
Wood	2.19E-11	3.51E-13	3.87E-13	1.41E-11	9.48E-14	7.68E-14	-3.55E-13
Wind	0.27	2.82E-03	6.00E-03	0.18	1.47E-03	1.24E-03	-7.03E-03
Other renew- able fuels	0.00	0.00	0.00	0.00	0.00	0.00	0.00
Total	88.47	0.27	0.15	2.39	1.80	0.15	-0.35

Table 12: Contribution of life cycle stages to total primary energy demand (gross calorific values) per 1 kg ABS, see Figure 3

Total Pri- mary Energy [MJ]	Precursors	Other Chemicals	Utilities	Electricity	Thermal Energy	Transport	Process Waste Treatment
Coal	1.33	0.06	0.17	0.16	1.96E-03	1.52E-03	-9.59E-03
Oil	46.61	0.81	0.19	0.06	5.41E-03	0.03	7.25E-04
Natural gas	33.94	0.78	0.31	1.60	1.74	4.71E-03	-0.10
Lignite	0.48	0.05	0.16	0.01	8.68E-04	1.28E-03	-8.44E-03
Nuclear	1.13	0.06	0.22	0.77	2.73E-03	2.70E-03	-0.02
Biomass	0.00	0.00	0.00	0.00	0.00	0.00	0.00
Hydro	0.17	1.05E-02	3.41E-02	0.05	5.33E-04	5.21E-04	-4.55E-03
Solar	0.29	0.53	6.00E-02	0.10	7.88E-04	8.91E-04	-3.32E-03
Geothermics	7.55E-03	1.82E-04	1.07E-03	3.14E-03	6.77E-05	2.27E-05	-2.09E-04
Waves	1.94E-13	1.40E-14	4.51E-14	6.20E-14	4.56E-16	2.55E-16	-1.51E-15
Wood	1.79E-11	1.29E-12	4.14E-12	5.72E-12	4.46E-14	2.35E-14	-1.39E-13
Wind	0.24	1.09E-02	3.91E-02	7.09E-02	6.01E-04	3.79E-04	-2.93E-03
Other renew- able fuels	0.00	0.00	0.00	0.00	0.00	0.00	0.00
Total	84.19	2.31	1.20	2.83	1.75	0.05	-0.15

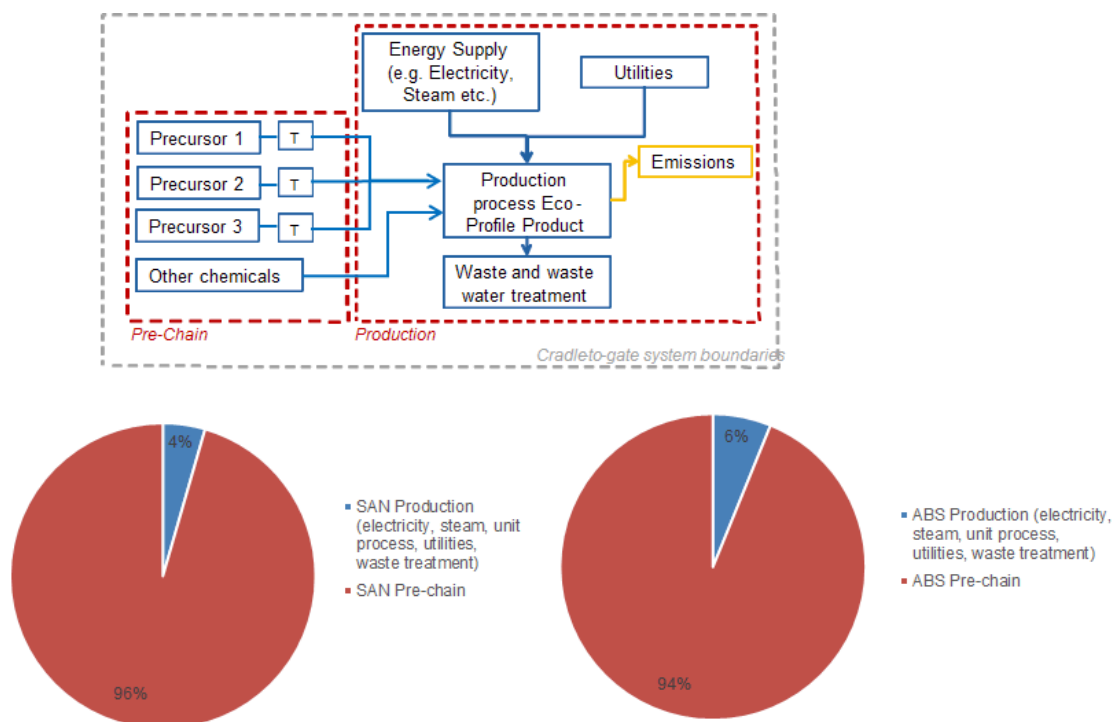


Figure 3: Contribution to primary energy demand per segment

Water Consumption

Table 13 and Table 14 show the water use at cradle-to-gate level. Water use (incl. fresh- and seawater; blue- and green water) equals the measured water input into a product system or process. Water use is determined by total water withdrawal (water abstraction).

Table 13: Water use (fresh- and seawater; blue- and greenwater) table per 1 kg SAN (cradle-to-gate)

Input	Value [kg]
Water (ground water)	11.11
Water (lake water)	49.13
Water (rain water)	2.67
Water (river water)	716.28
Water (sea water)	3.24
Water (fossil groundwater)	0.00
Overall water use [kg]	782.43

Table 14: Water use (fresh- and seawater; blue- and greenwater) table per 1 kg ABS (cradle-to-gate)

Input	Value [kg]
Water (ground water)	26.49
Water (lake water)	45.34
Water (rain water)	10.63
Water (river water)	738.63
Water (sea water)	3.03
Water (fossil groundwater)	0.00
Overall water use [kg]	824.14

Table 15 and Table 16 provide the corresponding freshwater part in the water balance. Freshwater is naturally occurring water on the Earth's surface in ponds, lakes, rivers and streams, as ice, and underground as groundwater in aquifers and underground streams. The term specifically excludes seawater and brackish water. Blue water refers to surface and groundwater used.

Table 15: Freshwater (blue water not including rain water) use table per 1 kg SAN (cradle-to-gate), see

Input	Value [kg]
Water (ground water)	11.11
Water (lake water)	49.13
Water (river water)	716.28
Water (fossil groundwater)	0.00
Total fresh water use [kg]	776.52

Output	Value [kg]
Water (river water from technosphere, cooling water)	40.64
Water (river water from technosphere, turbined)	718.96
Water (river water from technosphere, waste water)	4.46
Water (lake water from technosphere, cooling water)	0.00
Water (lake water from technosphere, turbined)	0.00
Water (lake water from technosphere, waste water)	0.00
Total fresh water release from technosphere (degradative use) [kg]	764.06
Total fresh water consumption (blue water)	12.46

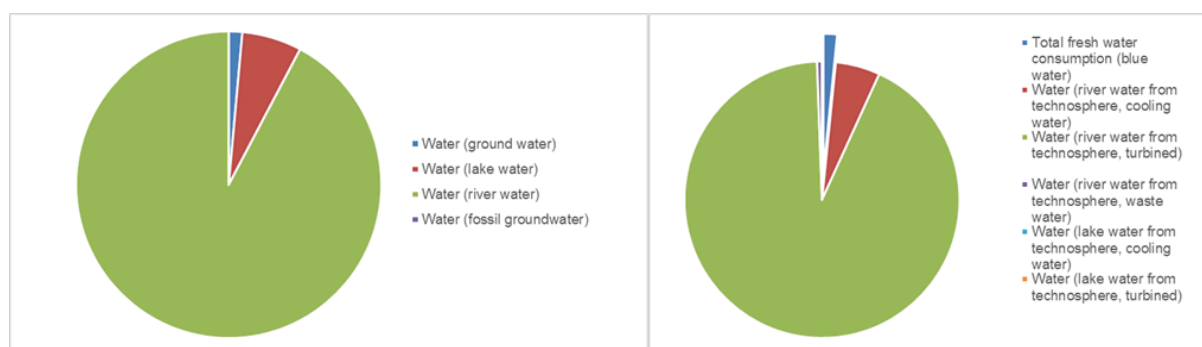


Figure 4: Total fresh water use (input) / water release (output) and water consumption (SAN)

Table 16: Freshwater (blue water not including rain water) use table per 1 kg ABS (cradle-to-gate), see

Input	Value [kg]
Water (ground water)	26.49
Water (lake water)	45.34
Water (river water)	738.63
Water (fossil groundwater)	0.00
Total fresh water use [kg]	810.47
<hr/>	
Output	Value [kg]
Water (river water from technosphere, cooling water)	39.53
Water (river water from technosphere, turbined)	741.49
Water (river water from technosphere, waste water)	7.25
Water (lake water from technosphere, cooling water)	0.00
Water (lake water from technosphere, turbined)	0.00
Water (lake water from technosphere, waste water)	0.00
Total fresh water release from technosphere (degradative use) [kg]	788.28
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Total fresh water consumption (blue water)	22.19

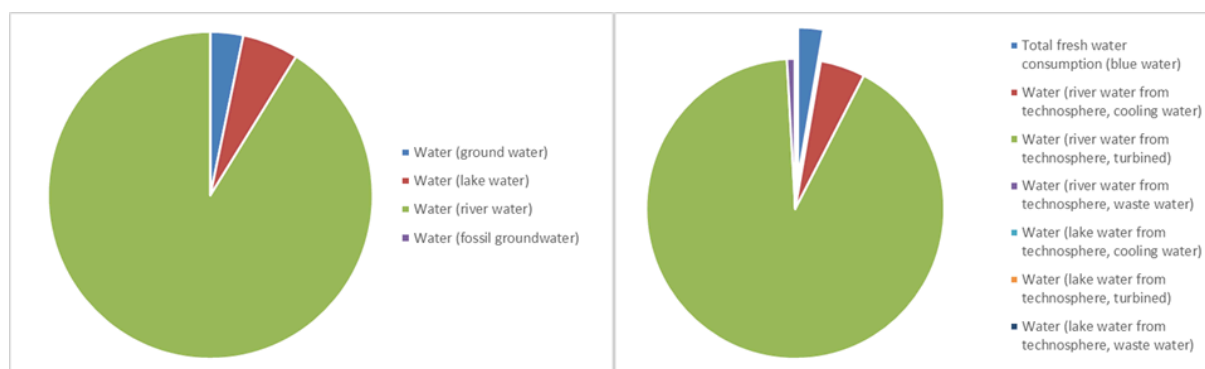


Figure 5: Total fresh water use (input) / water release (output) and water consumption (ABS)

Table 17 and Table 18 show the water balance at key foreground process level.

Table 17: Water balance table per 1 kg SAN (key foreground process level)

Input	Value [kg]
Water (cooling water) ⁴	0.00
Water (process water)	0.05
Water (deionised)	0.07
Water (tap water)	0.00
Water (ground water)	14.63
Water (river water)	7.02
Water (sea water)	0.00
Total water input	21,76
Output	Value [kg]
Water vapour	2.48
Water (waste water, untreated) to WWTP	0.72
<u>Water direct released to the environment without WWTP</u>	
Water (river water from technosphere, cooling water)	18.72
Water (river water from technosphere, turbinised)	0.00
Water (river water from technosphere, waste water)	0.00
Water (sea water from technosphere, cooling water)	0.00
Water (sea water from technosphere, turbinised)	0.00
Water (sea water from technosphere, waste water)	0.00
Water (lake water from technosphere, cooling water)	0.00
Water (lake water from technosphere, turbinised)	0.00
Total water output	21.92

⁴ Cooling water can be processed (softened), deionised, tap, ground, river or sea water, dependent on the location, applied technology and necessary temperature level and site specific frame conditions. Data for differentiation of water amounts used for cooling and processing due to lack of specific meters only partly available.

Table 18: Water balance table per 1 kg ABS (key foreground process level)

Input	Value [kg]
Water (cooling water) ⁴	0.00
Water (process water)	12.50
Water (deionised)	0.65
Water (tap water)	0.00
Water (ground water)	0.00
Water (river water)	8.88
Water (sea water)	0.00
Total water input	22.03
Output	Value [kg]
Water vapour	11.73
Water (waste water, untreated) to WWTP	1.71
<u>Water direct released to the environment without WWTP</u>	
Water (river water from technosphere, cooling water)	8.88
Water (river water from technosphere, turbinised)	0.00
Water (river water from technosphere, waste water)	0.00
Water (sea water from technosphere, cooling water)	0.00
Water (sea water from technosphere, turbinised)	0.00
Water (sea water from technosphere, waste water)	0.00
Water (lake water from technosphere, cooling water)	0.00
Water (lake water from technosphere, turbinised)	0.00
Total water output	22.33

Air Emission Data

Table 19 and Table 20 show a few selected air emissions which are commonly reported and used as key performance indicators; for a full inventory of air emissions, please refer to the complete LCI table in the annex of this report.

Table 19: Selected air emissions per 1 kg SAN

Air emissions	kg
Carbon dioxide, fossil (CO ₂ , fossil)	2.68
Carbon monoxide (CO)	1.40E-03
Methane (CH ₄)	9.01E-03
Sulphur dioxide (SO ₂)	3.99E-03
Nitrogen oxides (NO _x)	6.16E-03
Particulate matter • 10 µm (PM 10)	1.37E-07

Table 20: Selected air emissions per 1 kg ABS

Air emissions	kg
Carbon dioxide, fossil (CO ₂ , fossil)	2.81
Carbon monoxide (CO)	1.69E-03
Methane (CH ₄)	8.65E-03
Sulphur dioxide (SO ₂)	3.75E-03
Nitrogen oxides (NO _x)	5.48E-03
Particulate matter • 10 µm (PM 10)	2.35E-07

Wastewater Emissions

Table 21 and Table 22 show a few selected wastewater emissions which are commonly reported and used as key performance indicators; for a full inventory of wastewater emissions, please refer to the complete LCI table in the annex of this report.

Table 21: Selected water emissions per 1 kg SAN

Water emissions	kg
Biological oxygen demand after 5 days (BOD 5)	3.50E-05
Chemical oxygen demand (COD)	6.74E-04
Total organic carbon (TOC)	2.52E-05

Table 22: Selected water emissions per 1 kg ABS

Water emissions	kg
Biological oxygen demand after 5 days (BOD 5)	5.94E-05
Chemical oxygen demand (COD)	7.06E-04
Total organic carbon (TOC)	4.56E-05

Solid Waste

Table 23: Solid waste generation per 1 kg SAN (key foreground process level)

Waste for –	Incineration kg	Landfill kg	Recovery kg	Unspecified kg	Total kg
Non-hazardous	0.00	0.00	0.00	0.00	0.00
Hazardous	0.00	0.00	0.00	0.00	0.00
Unspecified	1.22E-02	0.00	5.57E-03	0.00	1.82E-02
Total	1.22E-02	0.00	5.57E-03	0.00	1.82E-02

Table 24: Solid waste generation per 1 kg ABS (key foreground process level)

Waste for –	Incineration kg	Landfill kg	Recovery kg	Unspecified kg	Total kg
Non-hazardous	0.00	0.00	0.00	0.00	0.00
Hazardous	0.00	0.00	0.00	0.00	0.00
Unspecified	6.08E-03	0.00	1.02E-03	0.00	8.28E-03
Total	6.08E-03	0.00	1.02E-03	0.00	8.28E-03

The End-of-life scenarios for different waste fractions is considered in partial stream calculations; i.e. the resource depletion and emissions referring to incineration and landfilling and the respective credits for energy gain depend on calorific value and actual elementary composition, which is relevant for the life cycle assessment. This is independent from the official attribution into hazardous/non-hazardous categories not consistently provided in the data collection.

Life Cycle Impact Assessment

The results for the impact assessment are calculated applying characterisation factors according CML 2001, latest update April 2013.

Input

Natural Resources

Table 25: Abiotic Depletion Potential per 1 kg SAN

Natural resources	Value
Abiotic Depletion Potential (ADP), elements [kg Sb eq]	8.87E-07
Abiotic Depletion Potential (ADP), fossil fuels [MJ]	82.93

Table 26: Abiotic Depletion Potential per 1 kg ABS

Natural resources	Value
Abiotic Depletion Potential (ADP), elements [kg Sb eq]	1.48E-06
Abiotic Depletion Potential (ADP), fossil fuels [MJ]	81.37

Output

Climate Change

Table 27: Global Warming Potential (100 years) per 1 kg SAN

Climate change	kg CO ₂ eq.
Global Warming Potential (GWP)	2.96

Table 28: Global Warming Potential (100 years) per 1 kg ABS

Climate change	kg CO ₂ eq.
Global Warming Potential (GWP)	3.10

Acidification

Table 29: Acidification Potential per 1 kg SAN

Acidification of soils and water bodies	g SO ₂ eq.
Acidification Potential (AP)	8.04

Table 30: Acidification Potential per 1 kg ABS

Acidification of soils and water bodies	g SO ₂ eq.
Acidification Potential (AP)	7.69

Eutrophication

Table 31: Eutrophication Potential per 1 kg SAN

Eutrophication of soils and water bodies	g PO ₄ ³⁻ eq.
Eutrophication Potential (EP), total	1.02

Table 32: Eutrophication Potential per 1 kg ABS

Eutrophication of soils and water bodies	g PO ₄ ³⁻ eq.
Eutrophication Potential (EP), total	1.03

Ozone Depletion

Table 33: Ozone Depletion Potential per 1 kg SAN

	g CFC-11 eq.
Ozone Depletion Potential (ODP)	8.32E-08

Table 34: Ozone Depletion Potential per 1 kg ABS

	g CFC-11 eq.
Ozone Depletion Potential (ODP)	2.60E-07

Summer Smog

Table 35: Photochemical Ozone Creation Potential per 1 kg SAN

	g Ethene eq.
Photochemical Ozone Creation Potential	1.19

Table 36: Photochemical Ozone Creation Potential per 1 kg ABS

	g Ethene eq.
Photochemical Ozone Creation Potential	1.09

Dust & Particulate Matter

Table 37: *PM10 emissions per 1 kg SAN*

Particulate matter	g PM10 eq.
Particulate matter ≤ 2.5 µm	6.94E-02
Particulate matter 2.5-10 µm	9.82E-02
Particulate matter ≤ 10 µm	1.37E-04
Particulate matter > 10 µm	4.56E-02
Particulate matter total	2.13E-01

Table 38: *PM10 emissions per 1 kg ABS*

Particulate matter	g PM10 eq.
Particulate matter ≤ 2.5 µm	7.11E-02
Particulate matter 2.5-10 µm	1.25E-01
Particulate matter ≤ 10 µm	2.35E-04
Particulate matter > 10 µm	4.23E-02
Particulate matter total	2.39E-01

Dominance Analysis

Table 39 and Table 40 show the main contributions to the results presented above. A weighted average of the participating producers is used. Regarding SAN/AMSAN, in all analysed environmental impact categories, the pre-cursors styrene/alpha-methyl styrene and acrylonitrile contributes to more than 91% of the overall impact. Regarding ABS, most of the environmental impact categories are dominated by the pre-cursors styrene, acrylonitrile and (poly)butadiene (> 82%). For ABS: The production of deionised water, included in the group “Utilities” requires salt, which influences the impact category ADP elements significantly. The group “Other chemicals” covers additives, which also show significant influence to the category ADP elements.

Electrical and thermal energy of the considered foreground production process contributes significantly.

Table 39: *Dominance analysis of impacts per 1 kg SAN*

	Total Primary Energy [MJ]	ADP Elements [kg Sb eq.]	ADP Fossil [MJ]	GWP [kg CO ₂ eq.]	AP [g SO ₂ eq.]	EP [g PO ₄ ³⁻ eq.]	POCP [g Ethene eq.]
Pre-cursors and Process	95.25%	94.02%	96.24%	91.06%	92.40%	92.65%	95.77%
Other chemicals	0.29%	2.49%	0.23%	0.28%	0.43%	1.08%	0.22%
Utilities	0.16%	0.60%	0.09%	0.23%	0.39%	0.19%	0.16%
Electricity	2.57%	2.45%	1.62%	3.80%	3.13%	2.41%	1.63%
Thermal Energy	1.94%	0.37%	1.95%	3.36%	1.16%	0.96%	1.48%
Transport	0.16%	0.05%	0.16%	0.35%	2.95%	2.45%	1.00%
Process waste treatment	-0.37%	0.01%	-0.29%	0.91%	-0.48%	0.27%	-0.26%
Total	100.00%	100.00%	100.00%	100.00%	100.00%	100.00%	100.00%

Table 40: Dominance analysis of impacts per 1 kg ABS

	Total Primary Energy [MJ]	ADP Elements [kg Sb eq.]	ADP Fossil [MJ]	GWP [kg CO ₂ eq.]	AP [g SO ₂ eq.]	EP [g PO ₄ ³⁻ eq.]	POCP [g Ethene eq.]
Pre-cursors and Process	91.34%	45.19%	93.23%	89.48%	87.62%	82.70%	93.36%
Other chemicals	2.51%	18.98%	1.92%	1.18%	6.00%	9.79%	2.33%
Utilities	1.30%	34.62%	0.95%	2.11%	2.47%	2.84%	1.35%
Electricity	3.07%	0.89%	2.05%	3.52%	2.27%	1.91%	1.61%
Thermal Energy	1.90%	0.15%	1.94%	3.04%	0.98%	1.00%	1.23%
Transport	0.05%	0.01%	0.05%	0.10%	0.79%	0.64%	0.22%
Process waste treatment	-0.17%	0.17%	-0.14%	0.57%	-0.12%	1.12%	-0.09%
Total	100.00%	100.00%	100.00%	100.00%	100.00%	100.00%	100.00%

Comparison of the Present Eco-profile with its Previous Version (2005)

Table 41 and Table 42 compare the present results with the previous version of the Eco-profiles of SAN and ABS.

Table 41: Comparison of the present Eco-profile of SAN with its previous version (2005)

Environmental Impact Categories	Eco-profile SAN (2005)	Eco-profile SAN (2014)	Difference
Gross primary energy from resources [MJ]	94.29	91.61	-2.8%
Abiotic Depletion Potential (ADP), elements [kg Sb eq.]	5.36E-07	8.87E-07	65.6%
Abiotic Depletion Potential (ADP), fossil fuels [MJ]	84.88	82.93	-2.3%
Global Warming Potential (GWP) [kg CO ₂ eq.]	3.47	2.96	-14.5%
Acidification Potential (AP) [g SO ₂ eq.]	8.32	8.04	-3.3%
Eutrophication Potential (EP) [g PO ₄ ³⁻ eq.]	0.77	1.02	32.7%
Ozone Depletion Potential (ODP) [g CFC-11 eq.]	-	8.32E-08	
Photochemical Ozone Creation Potential [g Ethene eq.]	1.15	1.19	4.0%

Table 42: Comparison of the present Eco-profile of ABS with its previous version (2005)

Environmental Impact Categories	Eco-profile ABS (2005)	Eco-profile ABS (2014)	Difference
Gross primary energy from resources [MJ]	98.47	90.57	-8.0%
Abiotic Depletion Potential (ADP), elements [kg Sb eq.]	1.502E-06	1.48E-06	-1.8%
Abiotic Depletion Potential (ADP), fossil fuels [MJ]	88.24	81.37	-7.8%
Global Warming Potential (GWP) [kg CO ₂ eq.]	3.80	3.10	-18.4%
Acidification Potential (AP) [g SO ₂ eq.]	12.38	7.69	-37.9%
Eutrophication Potential (EP) [g PO ₄ ³⁻ eq.]	1.31	1.03	-21.8%
Ozone Depletion Potential (ODP) [g CFC-11 eq.]	-	2.60E-07	
Photochemical Ozone Creation Potential [g Ethene eq.]	1.47	1.09	-25.7%

Table 41 and Table 42 show a significant reduction of the environmental impact of both SAN and ABS between the two versions. Since the previous model is unavailable for review, interpretations and explanations are based on the current results and PE INTERNATIONAL's experience.

The dominance analysis above shows that both pre-cursors' data and the energy data are significant for the Eco-profiles. Therefore, improvements in the performance of the supply chain processes as well as reduction of the consumed energy are reflected here.

The higher difference in percentage variation regarding ADP elements (SAN) should be treated with great caution. The absolute values are very small figures, hence the values are still displaying the same order of magnitude.

Other factors that have an influence on the current results in reference to the previous study can be qualitatively summarised as follows.

- Changes in the foreground and background system:
 - Higher efficiency due to plants with higher production capacities
 - Improvements in energy management in the supply chain and the processing itself
 - Changes in the energy carrier mix used in the overall process chain
 - Stricter pollution and emissions control, such as exhaust air purification (POCP)
 - Changes in the electricity grid mix, in particular electricity from renewables becoming relevant, caused improvements in all impact categories.
- Methodological changes:
 - Compared with the 2005 version, the system boundaries now include the waste treatment of all wastes occurring in the process, so that only elementary flows cross the system boundary: this causes small changes in all impact categories. Please note that for the sake of comparability, waste arising is also reported on a foreground unit process level.
 - More detailed data collection, e.g. so far unspecified VOC data is now replaced by data for specific emissions or at least NMVOC and methane emissions, leading to higher burdens in POCP results.


Reviews

Internal Independent Quality Assurance Statement

As part of the overall quality assurance during the preparation of this Eco-profile, *PE INTERNATIONAL AG* conducted an internal review of this work.

Internal Independent Quality Assurance Statement

On behalf of PE INTERNATIONAL AG and its subsidiaries

Document prepared by	Angela Schindler
Title	Project Manager
Signature	
Date	16.10.2014

Quality assurance by	Thilo Kupfer
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Date	22.10.2014

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External Independent Review Summary

The subject of this critical review is the development of the Eco-profile for Styrene Acrylonitrile (SAN) and Acrylonitrile Butadiene Styrene (ABS).

The review process included various meetings/web-conferences between the LCA practitioner and the reviewer, which encompassed a model and database review and spot checks of data and calculations. Furthermore, the final Eco-profile report was reviewed by the reviewer as well as industry participants involved in this project. All questions and recommendations were discussed with the LCA practitioner, and the report was adapted and revised accordingly.

Primary industry data were collected for the foreground processes comprising the production of SAN and ABS and taking into account the specific production processes of the four participating companies. Background data representing the main precursors as well as all other material and energy inputs were taken from the GaBi database. Primary industry data was collected from 5 sites producing SAN (one of which producing SAN from Alpha Methyl Styrene (AMS)) and five sites producing ABS, which lead to an estimated overall representativeness of >90% of the installed European SAN and ABS production capacity.

A critical aspect of the study is the use of the background dataset for butadiene which is an important component (10-25%) of ABS production. It is a general principle of PlasticsEurope Eco-profiles that up-to-date Eco-profiles for precursor products should be used, if available. However, due to inter-operability issues between different LCA softwares and databases, a lack of information with regards to some inventory flows (e.g. water flows) and the use of different types of butadiene for ABS production, the integration of the Eco-profile for butadiene (PlasticsEurope 2012) caused difficulties. Consequently, GaBi datasets for the different types of butadiene were used accompanied by a detailed sensitivity analysis with the Eco-profile for butadiene for the main impact categories (please refer to the relevant section in the main report for more information).

The potential environmental impacts for SAN and ABS are dominated by the precursor products styrene, acrylonitrile and butadiene (for ABS) across most impact categories. Electricity and thermal energy needed for SAN and ABS production also have a significant impact (about 7-8% for GWP). The results for ADP elements in case of ABS are also driven by the use of deionised water which requires salt.

The Eco-profile report also includes a comparison of the results with the previous version of the SAN and ABS Eco-profiles. However, due to reasons outlined in the main report, a detailed analysis of the reasons for the differences is difficult and should be treated with great caution.

The LCA practitioners have demonstrated very good competence and experience, with a track record of LCA projects in the chemical and plastics industry. The critical review confirms that this Eco-profile adheres to the rules set forth in the PlasticsEurope's Eco-profiles and Environmental Declarations – LCI Methodology and PCR for Uncompounded Polymer Resins and Reactive Polymer Precursors (PCR version 2.0, April 2011). As a result, this dataset is assessed to be a reliable and high quality representation of SAN and ABS produced in Europe.

Name and affiliation of reviewer:

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References

- BOUSTEAD 2005 SAN Boustead, I., Eco-profiles of the European Plastics Industry: Styrene-Acrylonitrile Copolymer (SAN), Plastics Europe, June 2005
- BOUSTEAD 2005 ABS Boustead, I., Eco-profiles of the European Plastics Industry: Acrylonitrile-Butadiene-Styrene Copolymer (ABS), Plastics Europe, March 2005
- ECO-PROFILE ETHYLENE&OTHER] IFEU, Eco-profile of the European Plastics Manufacturers: Ethylene, Propylene, Butadiene, Pyrolysis Gasoline, Ethylene Oxide (EO), Ethylene Glycols (MEG, DEG, TEG), November 2012
- EYERER 1996 Ganzheitliche Bilanzierung – Werkzeug zum Planen und Wirtschaften in Kreisläufen, 1996
- GABI 6 GaBi 6 dataset documentation for the software-system and databases, LBP, University of Stuttgart and PE INTERNATIONAL AG, Leinfelden-Echterdingen, 2013 (<http://documentation.gabi-software.com/>)
- GUINÉE ET AL. 2001 Guinée, J. et. al. Handbook on Life Cycle Assessment - Operational Guide to the ISO Standards. Centre of Environmental Science, Leiden University (CML); The Netherlands, 2001.
- GUINÉE ET AL. 2002 Handbook on Life Cycle Assessment: An operational Guide to the ISO Standards; Dordrecht: Kluwer Academic Publishers, 2002.
- HEIJUNGS 1992 Heijungs, R., J. Guinée, G. Huppes, R.M. Lankreijer, H.A. Udo de Haes, A. Wegener Sleeswijk, A.M.M. Ansems, P.G. Eggels, R. van Duin, H.P. de Goede, 1992: Environmental Life Cycle Assessment of products. Guide and Backgrounds. Centre of Environmental Science (CML), Leiden University, Leiden.
- HUIJBREGTS 1999 Huijbregts, M., 1999: Life cycle impact assessment of acidifying and eutrophying air pollutants. Calculation of equivalency factors with RAINS-LCA. Interfaculty Department of Environmental Science, Faculty of Environmental Science, University of Amsterdam, The Netherlands.
- HUIJBREGTS 2000 Huijbregts, M.A.J., 2000. Priority Assessment of Toxic Substances in the frame of LCA. Time horizon dependency of toxicity potentials calculated with the multi-media fate, exposure and effects model USES-LCA. Institute for Biodiversity and Ecosystem Dynamics, University of Amsterdam, Amsterdam, The Netherlands. (<http://www.leidenuniv.nl/interfac/cml/lca2/>).
- IPCC 2007 IPCC, 2007: Climate Change 2007: The Physical Science Basis. Contribution of Working Group I to the Fourth Assessment. Report of the Intergovernmental Panel on Climate Change. [Solomon, S., D. Qin, M. Manning, Z. Chen, M. Marquis, K.B. Averyt, M. Tignor and H.L. Miller (eds.)]. Cambridge University Press, Cambridge, United Kingdom and New York, NY, USA, 996 pp.
- ISO 14040: 2006 ISO 14040 Environmental Management – Life Cycle Assessment – Principles and Framework. Geneva, 2006
- ISO 14044: 2006 ISO 14044 Environmental management -- Life cycle assessment -- Requirements and guidelines. Geneva, 2006

ILCD 2010	European Commission (2010): ILCD Handbook – General guide for Life Cycle Assessment (LCA) – Detailed guidance
PLASTICSEUROPE 2011	Life Cycle Inventory (LCI) Methodology and Product Category Rules (PCR) for Uncompounded Polymer Resins and Reactive Polymer Precursors. Version 2.0, April 2011.
PLASTICSEUROPE 2012	Eco_profiles and Environmental Product Declarations of the European Plastics Manufacturers; Ethylene, Propylene, Butadiene, Pyrolysis Gasoline, Ethylene Oxide (EO), Ethylene Glycols (MEG, DEG, TEG), November 2012
ULLMANN 2010	Ullmann's Encyclopedia of Industrial Chemistry, John Wiley & Sons, Inc. , Hoboken / USA, 2010
WMO 2003	WMO (World Meteorological Organisation), 2003: Scientific assessment of ozone depletion: 2002. Global Ozone Research and Monitoring Project - Report no. 47. Geneva.

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